

An exact formula is obtained for the equilibrium temperature of a surface in a stream of hot gas. The heat-transfer coefficient is supposed known.

In the study of aerohydrodynamic heating it is frequently necessary to know the equilibrium temperature of a surface, T_{eq} , determined by the heat balance between convective heat flow and radiative transfer:

$$\alpha(T_e - T_{\text{eq}}) = \varepsilon\sigma T_{\text{eq}}^4. \quad (1)$$

Up to the present time this equation has been solved graphically, by the method of successive approximations, or by approximate formulas [1]. We present the derivation of an exact analytic formula for the equilibrium temperature of a surface when the heat-transfer coefficient α is known.

We transform Eq. (1) to the form

$$T_{\text{eq}}^4 + \frac{\alpha T_{\text{eq}}}{\varepsilon\sigma} - \frac{\alpha T_e}{\varepsilon\sigma} = 0. \quad (1')$$

The roots of this equation coincide with the roots of two quadratic equations [2]

$$T_{\text{eq}}^2 + A \frac{T_{\text{eq}}}{2} + y - \frac{\alpha}{A} = 0, \quad (2)$$

where $A = \pm\sqrt{8y}$ and y is the real root of the cubic equation

$$8y^3 + 8 \frac{\alpha T_e}{\varepsilon\sigma} y - \left(\frac{\alpha}{\varepsilon\sigma}\right)^2 = 0, \quad (3)$$

which reduces to

$$y^3 + 3py - 2q = 0. \quad (3')$$

Since the discriminant $D = q^2 + p^3 > 0$, Equation (3') has one real root which can be found from the Cardan solution: $y = u + v$, where

$$u = \sqrt[3]{-q + \sqrt{q^2 + p^3}}, \quad v = \sqrt[3]{-q - \sqrt{q^2 + p^3}}.$$

Consequently

$$y = \left[\frac{\alpha^2}{16 \varepsilon^2 \sigma^2} + \sqrt{\left(\frac{\alpha^2}{16 \varepsilon^2 \sigma^2}\right)^2 + \left(\frac{\alpha T_e}{3 \varepsilon \sigma}\right)^3} \right]^{1/3} + \left[\frac{\alpha^2}{16 \varepsilon^2 \sigma^2} - \sqrt{\left(\frac{\alpha^2}{16 \varepsilon^2 \sigma^2}\right)^2 + \left(\frac{\alpha T_e}{3 \varepsilon \sigma}\right)^3} \right]^{1/3}. \quad (4)$$

From (2) the equilibrium temperature is

$$T_{\text{eq}} = -\frac{A}{4} \pm \sqrt{\frac{A^2}{16} - \left(y - \frac{\alpha}{A\varepsilon\sigma}\right)}. \quad (5)$$

For $A = -\sqrt{8y}$ we obtain the two complex conjugate roots

$$T_{\text{eq}} = \sqrt{\frac{y}{2}} \pm \sqrt{\frac{y}{2} - \left(y + \frac{\alpha}{\varepsilon\sigma\sqrt{8y}}\right)} = \sqrt{\frac{y}{2}} \pm \sqrt{-\frac{y}{2} - \frac{\alpha}{\varepsilon\sigma\sqrt{8y}}}. \quad (6)$$

These roots do not correspond to the required real physical solution.

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For positive $A = \sqrt{8y}$

$$T_{eq} = -\sqrt{\frac{y}{2}} \pm \sqrt{-\frac{y}{2} + \frac{\alpha}{\varepsilon\sigma\sqrt{8y}}} \quad (7)$$

Since a positive solution is required and y , α , ε , and σ are positive at the equilibrium temperature, there remains the single real positive root

$$T_{eq} = -\sqrt{\frac{y}{2}} + \sqrt{-\frac{y}{2} + \frac{\alpha}{\varepsilon\sigma\sqrt{8y}}} \quad (8)$$

Similarly an analytic formula can be obtained for the steady-state temperature of a wall heated by a stream of hot gas on the outside, and cooled from the inside. Thus, for example, for the steady removal of heat through a wall with a heat-transfer coefficient α_{in} , the heat-balance equation has the form:

$$\alpha(T_e - T_{out}) = \varepsilon\sigma T_{out}^4 + \alpha_{in}(T_{out} - T_{in}), \quad (9)$$

and

$$\alpha_{in} = \frac{\lambda}{\delta}, \quad (10)$$

$$T_{out} = -\sqrt{\frac{y_1}{2}} + \sqrt{-\frac{y_1}{2} + \frac{\alpha + \alpha_{in}}{\varepsilon\sigma\sqrt{8y_1}}} \quad (11)$$

where

$$y_1 = \left[\frac{(\alpha + \alpha_{in})^2}{16\varepsilon^2\sigma^2} + \sqrt{\left[\frac{(\alpha + \alpha_{in})^2}{16\varepsilon^2\sigma^2} \right]^2 + \left(\frac{\alpha T_e + \alpha_{in} T_{in}}{3\varepsilon\sigma} \right)^3} \right]^{1/3} + \left[\frac{(\alpha + \alpha_{in})^2}{16\varepsilon^2\sigma^2} - \sqrt{\left[\frac{(\alpha + \alpha_{in})^2}{16\varepsilon^2\sigma^2} \right]^2 + \left(\frac{\alpha T_e + \alpha_{in} T_{in}}{3\varepsilon\sigma} \right)^3} \right]^{1/3} \quad (12)$$

NOTATION

T_{in}	is the temperature of the inside surface;
T_e	is the recovery temperature;
T_{out}	is the temperature of the outside surface;
T_{eq}	is the equilibrium temperature;
α	is the coefficient for heat transfer from the hot gas to the surface;
α_{in}	is the coefficient for heat transfer through the wall;
δ	is the wall thickness;
ε	is the emissivity;
λ	is the thermal conductivity;
σ	is the Stefan-Boltzmann constant.

LITERATURE CITED

1. N. F. Krasnov, *Aerodynamics of Bodies of Revolution*, Elsevier, New York (1970).
2. V. I. Smirnov, *A Course in Higher Mathematics [in Russian]*, Vol. 1, GIFML, Moscow (1961).